

**13th NATIONAL CERTIFICATION EXAMINATION
 FOR
 ENERGY MANAGERS & ENERGY AUDITORS - September 2012**

PAPER – 2: Energy Efficiency in Thermal Utilities			
Date: 15.9.2012	Timings:14:00-17:00Hrs	Duration:3 Hrs	Max.Marks:150

Section – I: OBJECTIVE TYPE

Marks: 50 x 1 = 50

- (i) Answer all **50** questions
- (ii) Each question carries **one** mark

1.	Which of the following is not true of condensate recovery? a) reduces water charges b) reduces fuel costs c) increases boiler output d) <u>increases boiler blow down</u>
2.	Which of the following is not a property of ceramic fibre ? a) low thermal conductivity b) light weight c) <u>high heat capacity</u> d) thermal shock resistant
3.	Which of the following is false? a) <u>LPG vapour is twice as light as air</u> b) LPG is a mixture of propane and butane c) LPG is a gas at normal atmospheric pressure d) LPG is required to be odorized
4.	Which of the following in fuel contributes to erosive effect on burner tips during combustion? a) <u>ash content</u> b) water content c) sulphur content d) volatile matter
5.	Tuyeres is a terminology associated with a) induction furnace b) pusher type furnace c) arc furnace d) <u>cupola</u>
6.	Turn down ratio of a burner is the ratio of a) <u>maximum to minimum fuel input without affecting optimum excess air levels</u> b) minimum to maximum fuel input without affecting optimum excess air levels c) maximum to average fuel input d) average to minimum fuel input
7.	Time dependent property that determines the deformation of a refractory is a) <u>creep</u> b) refractoriness under load c) porosity d) crushing strength
8.	The working fluid for thermo compressor is a) low pressure steam b) <u>high pressure steam</u> c) compressed air d) waste heat from chimney

9.	The velocity of steam in steam pipe is directly proportional to a) number of bends in pipe c) length of pipe b) <u>specific volume of steam</u> d) diameter of the pipe
10.	The unit of specific gravity in SI system is a) kg/ m ³ b) m ³ /kg c) gm/cc d) <u>none of the above</u>
11.	The storage heat losses in a batch type furnace can be best reduced by a) insulating brick b) <u>ceramic fibre</u> c) cold face insulation d) fire brick
12.	The softening temperature of a refractory is indicated by a) <u>Pyrometric cone equivalent (PCE)</u> c) creep b) refractoriness under load (RUL) d) cold crushing strength
13.	The recommended TDS level for package fire tube boilers is a) 10,000 ppm b) 5,000 ppm c) 2,000 ppm d) <u>3,000 ppm</u>
14.	The presence of calcium and magnesium bicarbonates in feedwater to a boiler would form a) acidic solution b) <u>alkaline solution</u> c) neutral solution d) none of the above
15.	The mineral matter in coal after combustion mostly becomes a) carbon dioxide b) carbon monoxide c) nitrous oxide d) <u>ash</u>
16.	The emissivity of ceramic coatings used in furnace a) decreases with increase in furnace temperature b) <u>Increases with increase in furnace temperature</u> c) remains constant d) decreases with increase in furnace pressure
17.	The effectiveness of a heat exchanger does not depend on a) specific heat of hot fluid c) inlet temperature of hot fluid b) specific heat of cold fluid d) <u>LMTD</u>
18.	The device used for recovering waste heat from the textile drier exhaust is a) <u>heat wheel</u> b) recuperator c) economizer d) regenerator
19.	The cogeneration system which has high overall system efficiency is a) <u>back pressure steam turbine</u> c) extraction condensing steam turbine b) combined cycle d) reciprocating engine

20.	The Brayton cycle is a characteristic of a) steam turbine b) petrol engine c) <u>gas turbine</u> d) none of the above
21.	The amount of flash steam generated from the condensate depends on _____ a) sensible heat of high pressure condensate b) sensible heat of flash steam c) latent heat of flash steam d) <u>all of the above</u>
22.	Ten meter lift of condensate in a distribution pipe work will result in a) 0.1 bar back pressure b) <u>1 bar back pressure</u> c) 10 bar back pressure d) none of the above
23.	Steam mains are run with a slope primarily to a) <u>avoid water hammer</u> b) increase the velocity of steam c) avoid condensation of steam d) reduce radiation and convection losses
24.	Select the incorrect statement with respect to steam a) evaporation is a constant temperature process b) higher the pressure higher is the steam saturation temperature c) <u>higher the pressure higher is the latent heat</u> d) latent heat at critical point is zero
25.	Scale losses in reheating furnaces will a) <u>increase with excess air</u> b) decrease with excess air c) have no relation with excess air d) increase with CO in combustion gases
26.	Reduction of steam pressure will increase a) sensible heat b) enthalpy of steam c) saturation temperature d) <u>specific volume</u>
27.	Recuperator as a waste heat recovery system is used mainly in a a) boiler b) <u>reheating furnace</u> c) compressor d) gas turbine
28.	Power is to be generated from a cement kiln exhaust gas. The applicable type of cogeneration is called a) topping cycle b) trigeneration c) <u>bottoming cycle</u> d) none of the above
29.	Of the following fuels, which will have the highest carbon content? a) <u>furnace oil</u> b) coal c) natural gas d) paddy husk
30.	Low combustion temperature in FBC boilers results in the reduced formation of a) <u>NO_x</u> b) SO _x c) CO d) CO ₂
31.	Insulation used for temperatures more than 350°C is

	a) polyurethane	b) polystyrene	c) <u>calcium silicate</u>	d) wood
32.	Instrument used for measuring billet temperature in a reheating furnace is ____.			
	a) thermograph	b) <u>infrared pyrometer</u>		d) chrome alumel thermocouple with indicator
	c) Pt/Pt-Rh thermocouple with indicator			
33.	In the direct method of efficiency evaluation of boilers which of the following is not required?			
	a) enthalpy of steam	b) calorific value of fuel		d) mass flow rate of steam
	c) <u>O₂ in flue gas</u>			
34.	In the context of cogeneration turbine, the thermodynamic process taking place is			
	a) <u>expansion</u>	b) condensation	c) contraction	d) both (a) & (c)
35.	In determining the economic thickness of steam pipe insulation which of the following is not required?			
	a) cost of fuel	b) boiler efficiency	c) <u>steam pressure</u>	d) heat content of fuel
36.	If 10% air is entrained in a steam system at 3 kg/cm ² g then the saturation temperature of steam will be			
	a) <u>less than the saturation temperature at 3 kg/cm² g</u>			
	b) more than the saturation temperature at 3 kg/cm ² g			
	c) equal to the saturation temperature at 3 kg/cm ² g			
	d) equal to the saturation temperature at 3.3 kg/cm ² g			
37.	Ideal furnace for melting & alloying is			
	a) <u>induction furnace</u>	b) cupola furnace	c) rotary hearth	d) recirculating bogie furnace
38.	Heat transfer in a reheating furnace is achieved by			
	a) conduction	b) convection	c) radiation	d) <u>all of the above</u>
39.	Glass mineral wool can be applied for temperature range application upto			
	a) 950 °C	b) <u>500 °C</u>	c) 1200 °C	d) 750 °C
40.	Fly ash in a FBC boiler is in the range of			
	a) 20%	b) 30%	c) 40%	d) <u>none of the above</u>
41.	Dolomite is a _____ type of refractory			
	a) acidic	b) <u>basic</u>	c) neutral	d) none of the above

<p>Ans</p>	<p>a.</p> <p>‘lowest’ : Lower the pressure higher is the latent heat which is primarily used in the process. Hence the lowest pressure would be desirable.</p> <p>‘acceptable’: However the lower the steam pressure lower will be the steam temperature. Since the temperature is the driving force for heat transfer, rate of heat transfer reduces and increases process time. Therefore there is a limit to the reduction in steam pressure.</p> <p>b.</p> <p>Heat rate is the heat input to turbine, needed to produce 1 kWh of electricity</p> <p>Turbine efficiency is the ratio useful heat and power output, to the heat input to the turbine in Kcal or KJ, expressed as a percentage. Performance of steam turbine is also expressed as heat rate, which is the quantity of heat in kCal or KJ required to generate 1 kWh of electrical power output.</p> <p>Turbine heat rate is expressed in kJ/kWh. The inverse relation between heat rate and efficiency is applicable only to a power plant, since all the input energy is deployed for power generation alone.</p>
<p>S-2</p>	<p>A process requires 6.5 tons/hr of dry saturated steam at 7 kg/cm²g having specific volume of 0.28 m³/kg. For the flow velocity not to exceed 25 m/s, determine the pipe diameter.</p>
<p>Ans</p>	<p>Volumetric flow rate = 6500 x 0.28 = 1820 m³/hr = 1820/3600 = 0.505 m³/s</p> <p>Cross sectional area = volumetric flow rate / velocity = 0.505 / 25</p> <p>$3.14 \times D^2/4 = 0.0202$ $D^2 = 0.0257$ Diameter, D = 0.160 m (or) 160 mm</p>
<p>S-3</p>	<p>A vessel has to be cooled from 90°C to 45°C. The mass of the vessel is 2 tonnes. The specific heat of vessel material is 0.18 kCal/kg °C. The vessel is cooled with water which is available at 28°C. The maximum allowed increase in water temperature is 6°C. Calculate the quantity of water required for vessel cooling.</p>

<p>Ans</p>	<p> Mass of vessel (m) = 2000 kg Specific heat (Cp) = 0.18 kCal/kg °C Initial vessel temperature (T1) = 90°C Desired vessel temperature (T2) = 45°C </p> <p> Total heat that has to be removed from the vessel = $m \times Cp \times (T1 - T2)$ $= 2000 \times 0.18 \times (90-45)$ $= 16200 \text{ kCal}$ </p> <p> Quantity of water required = M kg Specific heat of water = 1 kCal/kg °C Inlet cooling water temperature (T3) = 28°C Maximum cooling water outlet temperature (T4) = 34°C Heat removed by water, $16200 = M \times 1 \times (34 - 28)$ </p> <p> Quantity of water required , $M = 12600/6 = 2700 \text{ kg}$ </p>
<p>S-4</p>	<p>a) 350 kg/hr of hot condensate from a heat exchanger is coming out at 6 bar(g) with a sensible heat of 166 kCal/kg. Using a flash vessel, the condensate is flashed to 1 bar(g) with a sensible heat of 120 kCal/kg and latent heat of 526 kCal/kg. Find out the flash steam generation in kg/hr.</p> <p>b) The flash steam produced above is used to heat water from 30°C to 80°C by direct injection. Calculate the quantity of hot water in that can be obtained per hour.</p>
<p>Ans</p>	<p>a) Flash steam available % $= (S1 - S2) / L2$</p> <p> S1 = is the sensible heat of higher pressure steam S2 = is the sensible heat of the steam at lower pressure L2 = is the latent heat of flash steam (at lower pressure) </p> <p> Flash Steam generated $= \frac{(166 - 120) \times 350}{526}$ $= 30.6 \text{ Kg/hr.}$ </p> <p>b) Quantity of hot water generated</p> <p> $m \times cp \times (80-30) = 30.6 \times (120+526)$ $m = 395 \text{ kg/hr}$ </p>
<p>S-5</p>	<p>Explain any two proven methods of testing steam traps?</p>

ANS	<p>There are two proven methods of testing of steam traps: - Sound method and Temperature method.</p> <p>1.Sound Method : Mechanisms within steam traps and the flow of steam and condensate through steam traps generate sonic (audible to the human ear) and supersonic sounds. Proper listening equipment, coupled with the knowledge of normal and abnormal sounds, can yield reliable assessments of steam trap working condition. Listening devices range from a screwdriver or simple mechanic's stethoscope that allow listening to sonic sounds.</p> <p>2.Temperature Method: Saturated steam and condensate exist at the same temperature. So it's not possible to distinguish between the two based on temperature. Still, temperature measurement provides important information for evaluation purposes.</p> <p>A cold trap (i.e., one that is significantly cooler than the expected saturated steam temperature) indicates that the trap is flooded with condensate, assuming the trap is in service. On the other hand, the temperature downstream of the trap will be nearly constant if significant steam is getting past the trap. At the low-end, spitting on the trap and watching the sizzle provides a general indication of temperature.</p> <p>Finally, non-contact (i.e., infrared) temperature measuring devices provide the precision of thermometers and thermocouples without requiring physical contact. Non-contact temperature measurement makes it easier to evaluate traps that are relatively difficult or dangerous to access closely.</p>													
S-6	<p>In a paper industry, 35,000 kg/hr of soda liquor with specific heat of 0.38 kCal/kg°C is heated using saturated steam at 8 bar in a heat exchanger from 60°C to 120°C. Calculate the LMTD of the exchanger & the amount of steam required for heating using the following data:</p> <table border="1" data-bbox="444 1314 1183 1493"> <thead> <tr> <th rowspan="2">Steam Pressure (bar)</th> <th rowspan="2">Steam Temperature °C</th> <th colspan="3">Enthalpy kcal/kg</th> </tr> <tr> <th>Water</th> <th>Evaporation</th> <th>Steam</th> </tr> </thead> <tbody> <tr> <td>8.0</td> <td>170</td> <td>170</td> <td>490</td> <td>660</td> </tr> </tbody> </table>	Steam Pressure (bar)	Steam Temperature °C	Enthalpy kcal/kg			Water	Evaporation	Steam	8.0	170	170	490	660
Steam Pressure (bar)	Steam Temperature °C			Enthalpy kcal/kg										
		Water	Evaporation	Steam										
8.0	170	170	490	660										

Ans	<p>a) Heat gain by soda liquor = $35000 \times 0.38 \times (120-60)$ = 798000 Kcal/hr Heat lost by saturated steam = 798000 Kcal/hr Steam required for heating = $798000 / 490$ = 1628 Kg/hr Amount of steam required for heating is 1.63 Ton/hr</p> <p>b) LMTD calculation = $\frac{(170-120)-(170-60)}{\ln \frac{(170-120)}{(170-60)}}$ = $(50-110)/\ln(50/110)$ = 76.1°C</p>
S-7	Write short notes on factors affecting wall losses in batch type reheating furnaces?
Ans	<p>a) Emissivity of walls : Emissivity of fire brick refractory should be high Emissivity of most of the refractory bricks decreases with increase in temperature. High emissivity coatings whose emissivity increases with temperature can be used to increase emissivity and decrease wall losses.</p> <p>b) Conductivity of refractories: The refractory and insulating bricks should have low thermal conductivity. Choosing low thermal conductivity bricks will reduce wall losses. Conductivity raises with rise in temperature. Batch type furnaces can use ceramic fibre to reduce storage losses.</p> <p>c) Wall thickness of Wall thickness of batch furnaces: Heat losses can be reduced by increasing the wall thickness, or through the application of insulating bricks. Outside wall temperature and heat losses for a composite wall of a certain thickness of firebrick and insulation brick are much lower due to lesser conductivity of may be worked out to reduce the heat storage.</p>
S-8	<p>The evaporation ratio of a coal fired boiler is 4.50. A quantity of 600 kCal/kg of heat is added to the feed water in the boiler to produce the steam.</p> <p>a) If the GCV of coal is 3800 kCal/kg, find out the boiler efficiency. b) Find out the total enthalpy of the steam as per the details of the data given below</p> <p>Saturation temperature = 143°C Sensible heat = 143.7 kCal/kg Latent heat = 509.96 kCal/kg Specific volume = 0.47 m³/kg Dryness fraction of steam = 92%</p>

Ans	<p>a) Boiler efficiency (%) = $\frac{\text{Evaporation ratio} \times \text{enthalpy added}}{\text{GCV of coal}} \times 100$</p> <p>Boiler efficiency = $4.5 \times 600 / 3800$ = 71 %</p> <p>b) Total enthalpy of steam = $143.7 + (0.92 \times 509.96)$ = 612.86 kCal/kg</p>
-----	------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------

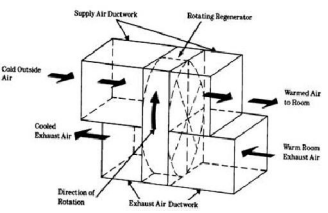
----- End of Section - II -----

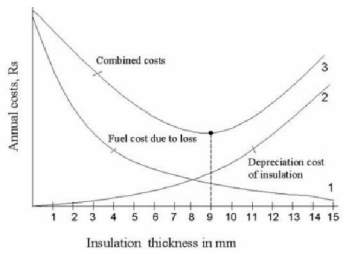
Section - III: LONG DESCRIPTIVE QUESTIONS

Marks: 6 x 10 = 60

- (i) Answer all 6 questions
- (ii) Each question carries 10 marks

L-1	<p>a) Find out the efficiency of the furnace oil fired boiler by direct method in a agro product manufacturing plant with the data given below:</p> <table style="width: 100%; border: none;"> <tr> <td>Type of boiler</td> <td>: Furnace oil fired</td> </tr> <tr> <td>Quantity of steam (dry) generated</td> <td>: 5 Ton per hour (TPH)</td> </tr> <tr> <td>Steam pressure / temp</td> <td>: 10 kg/cm²(g)/ 180 °C</td> </tr> <tr> <td>Quantity of oil consumed</td> <td>: 0.350 TPH</td> </tr> <tr> <td>Feed water temperature</td> <td>: 75 °C</td> </tr> <tr> <td>GCV of Furnace oil</td> <td>: 10400 kCal/kg</td> </tr> <tr> <td>Enthalpy of saturated steam at 10 kg/cm²</td> <td>: 665 kCal/kg</td> </tr> <tr> <td>Enthalpy of feed water</td> <td>: 75 kCal/kg</td> </tr> </table> <p>b) The above furnace oil fired boiler was replaced by a new coconut shell fired boiler. Determine the boiler efficiency of the new coconut shell fired boiler by direct method</p> <table style="width: 100%; border: none;"> <tr> <td>GCV of coconut shell fuel</td> <td>: 4565 kCal/kg</td> </tr> <tr> <td>Quantity of coconut shell consumed for the same steam demand and pressure.</td> <td>: 850 kg/hr</td> </tr> </table> <p>c) The cost of fuel and operating hour of boiler are given below.</p> <ul style="list-style-type: none"> • Operating hour/ year = 7000 hr • Cost of furnace oil per ton = Rs 40000/ton • Cost of coconut per ton = Rs 5000/ton <p>Find out the annual cost saving due to boiler replacement and fuel substitution?</p>	Type of boiler	: Furnace oil fired	Quantity of steam (dry) generated	: 5 Ton per hour (TPH)	Steam pressure / temp	: 10 kg/cm ² (g)/ 180 °C	Quantity of oil consumed	: 0.350 TPH	Feed water temperature	: 75 °C	GCV of Furnace oil	: 10400 kCal/kg	Enthalpy of saturated steam at 10 kg/cm ²	: 665 kCal/kg	Enthalpy of feed water	: 75 kCal/kg	GCV of coconut shell fuel	: 4565 kCal/kg	Quantity of coconut shell consumed for the same steam demand and pressure.	: 850 kg/hr
Type of boiler	: Furnace oil fired																				
Quantity of steam (dry) generated	: 5 Ton per hour (TPH)																				
Steam pressure / temp	: 10 kg/cm ² (g)/ 180 °C																				
Quantity of oil consumed	: 0.350 TPH																				
Feed water temperature	: 75 °C																				
GCV of Furnace oil	: 10400 kCal/kg																				
Enthalpy of saturated steam at 10 kg/cm ²	: 665 kCal/kg																				
Enthalpy of feed water	: 75 kCal/kg																				
GCV of coconut shell fuel	: 4565 kCal/kg																				
Quantity of coconut shell consumed for the same steam demand and pressure.	: 850 kg/hr																				

<p>ANS</p>	<p>a)Boiler efficiency with furnace oil firing :</p> <p>Boiler Efficiency (η) = $5000 \times (665-75) \times 100 / (350 \times 10400)$ Boiler efficiency = 81% (on GCV basis)</p> <p>b)Boiler efficiency with coconut shell fuel firing :</p> <p>Boiler Efficiency (η) = $5000 \times (665-75) / (850 \times 4565)$ Boiler efficiency = 76% (on GCV basis)</p> <p>c) Annual cost saving</p> <p>Annual furnace oil cost = $7000\text{Hr} \times 0.35 \times \text{Rs } 40000$ = Rs.9.8 crore</p> <p>Annual coconut shell Cost = $7000 \text{ hrs} \times 0.85 \times \text{Rs.}5000$ = Rs. 2.975 crore</p> <p>Annual cost saving = $9.8 - 2.975 = \text{Rs } 6.825 \text{ Crore}$</p>
<p>L2</p>	<p>Explain briefly <u>any two</u> of the following</p> <ol style="list-style-type: none"> Heat Wheel Topping and bottoming cycles for cogeneration with examples Economic thickness of insulation
<p>Ans</p>	<p>a) Heat wheel</p>  <p>Widely used in low to medium temperature waste heat recovery systems.</p> <p>A disk rotates between two side-by-side ducts: one a cold gas duct, the other a hot gas duct.</p> <p>As the disk slowly rotates, sensible heat (moisture that contains latent heat) is transferred to the disk by the hot air and, as the disk rotates, from the disk to the cold air.</p> <p>b) Topping and bottoming cycles for cogeneration with examples</p> <p>In a topping cycle, the fuel supplied is used to first produce power and then thermal energy, which is the by-product of the cycle and is used to satisfy process heat or other thermal</p>

	<p>requirements ex. steam turbine, Diesel engine, Gas turbine etc.</p> <p>In a bottoming cycle, the primary fuel produces high temperature thermal energy and the heat rejected from the process is used to generate power through a recovery boiler and a turbine generator Power production from waste heat of cement plant, sponge iron plant etc</p> <p>c) Economic thickness of insulation</p>  <p>As the insulation thickness increases heat loss cost reduces, At the same time insulation cost increases. Hence there is an optimum limit to thickness. The economic thickness of insulation is the thickness at which the combined cost is least.</p>
<p>L-3</p>	<p>In a crude distillation unit of a refinery, furnace is operated to heat 500 m³/hr of crude oil from 255°C to 360°C by firing 3.4 tons/hr of fuel oil having GCV of 9850 kcal/kg. As an energy conservation measure, the management has installed an air preheater (APH) to reduce the flue gas heat loss. The APH is designed to pre-heat 57 tonnes/hr of combustion air to 195°C.</p> <p>Calculate the efficiency of the furnace before & after the installation of APH.</p> <p>Consider the following data:</p> <ul style="list-style-type: none"> • Specific heat of crude oil = 0.6 kcal/kg°C • Specific heat of air = 0.24 kcal/kg°C • Specific gravity of Crude oil = 0.85 • Ambient temperature = 28°C.
<p>ANS</p>	<p><u>Before the installation of APH</u></p> <p>Heat gain by the crude = 500 x 1000 x 0.85 x 0.6 x (360-255) = 26775000 Kcal/hr</p> <p>Heat input to the furnace = 3.4 x 1000 x 9850 = 33490000 kcal/hr</p> <p>Efficiency of the furnace = 26775000 / 33490000 = 80 %</p> <p style="text-align: right;">5 marks</p> <p><u>After the installation of APH</u></p> <p>Heat gain by the crude = 500 x 1000 x 0.85 x 0.6 x (360-255) = 26775000 Kcal/hr</p> <p>Heat gain by Air-preheater = 57 x 1000 x 0.24 x (195-28) = 2284560 Kcal/hr</p>

	<p>Heat reduction in input to the furnace = Heat gain by Air-preheater</p> <p>New Heat input to the furnace = $33490000 - 2284560$ $= 31,205,440$</p> <p>Efficiency of furnace after installation of APH = $26775000 / 31,205,440$ $= 85.8 \%$</p>
L4	<p>List five energy conservation measures in ANY TWO of the following:</p> <p>a) Furnaces b) Steam distribution systems c) Boilers</p>
Ans	<p>a) Furnaces</p> <ol style="list-style-type: none"> 1) Complete combustion with minimum excess air 2) Correct heat distribution 3) Operating at the desired temperature 4) Reducing heat losses from furnace openings 5) Maintaining correct amount of furnace draught 6) Optimum capacity utilization 7) Waste heat recovery from the flue gases 8) Minimum refractory losses 9) Use of Ceramic Coatings <p>b) Steam Distribution systems</p> <ol style="list-style-type: none"> 1. Monitoring Steam Traps 2. Avoiding Steam Leakages 3. Providing Dry Steam for Process 4. Utilising Steam at the Lowest Acceptable Pressure for the Process 5. Minimising Heat Transfer Barriers 6. Proper Air Venting 7. Condensate Recovery 8. Insulation of Steam Pipelines and Hot Process Equipments 9. Flash Steam Recovery 10. Reducing the Work to be done by Steam <p>c) Boilers</p> <ol style="list-style-type: none"> 1. Reduce Stack Temperature 2. Feed Water Preheating using Economiser 3. Combustion Air Preheating 4. Ensure complete Combustion 5. Control excess air 6. Radiation and Convection Heat Loss 7. Automatic Blowdown Control 8. Reduction of Boiler Steam Pressure 9. Variable Speed Control for Fans, Blowers and Pumps 10. Ensure boiler Loading for Efficiency 11. Boiler Replacement for efficiency
L-5	<p>Paddy husk is being used as a fuel in a water tube boiler. The ultimate analysis of fuel is given below. Calculate the theoretical quantity of air required for complete combustion and also compute the quantity of CO₂, H₂O and SO₂ generated per 1000</p>

	<p>kg of fuel. The ultimate analysis of paddy husk is given below.</p> <table border="1"> <thead> <tr> <th>Ultimate analysis of paddy husk</th> <th>%</th> </tr> </thead> <tbody> <tr> <td>Moisture</td> <td>10.8</td> </tr> <tr> <td>Mineral Matter</td> <td>16.7</td> </tr> <tr> <td>Carbon</td> <td>34.0</td> </tr> <tr> <td>Hydrogen</td> <td>5.0</td> </tr> <tr> <td>Nitrogen</td> <td>0.9</td> </tr> <tr> <td>Sulphur</td> <td>0.1</td> </tr> <tr> <td>Oxygen</td> <td>32.5</td> </tr> <tr> <td>GCV (kCal/kg)</td> <td>3570</td> </tr> </tbody> </table>	Ultimate analysis of paddy husk	%	Moisture	10.8	Mineral Matter	16.7	Carbon	34.0	Hydrogen	5.0	Nitrogen	0.9	Sulphur	0.1	Oxygen	32.5	GCV (kCal/kg)	3570
Ultimate analysis of paddy husk	%																		
Moisture	10.8																		
Mineral Matter	16.7																		
Carbon	34.0																		
Hydrogen	5.0																		
Nitrogen	0.9																		
Sulphur	0.1																		
Oxygen	32.5																		
GCV (kCal/kg)	3570																		
ANS	<p>Considering a sample of 100 kg of paddy husk. The chemical reactions are:</p> <p>Oxygen required for complete combustion of carbon:</p> $\begin{array}{r} \text{C} + \text{O}_2 \rightarrow \text{CO}_2 \\ (34.0) \text{C} + (34 \times 2.67) \text{O}_2 \rightarrow \mathbf{124.78} \text{CO}_2 \\ \mathbf{90.78} \end{array}$ <p>Oxygen required for complete combustion of hydrogen:</p> $\begin{array}{r} \text{H}_2 + \text{O}_2 \rightarrow \text{H}_2\text{O} \\ (5) \text{H}_2 + (5 \times 8) \text{O}_2 \rightarrow \mathbf{45} \text{H}_2\text{O} \\ \mathbf{40} \end{array}$ <p>Oxygen required for complete combustion of sulphur:</p> $\begin{array}{r} \text{S} + \text{O}_2 \rightarrow \text{SO}_2 \\ (0.1) \text{S} + (0.1 \times 1) \text{O}_2 \rightarrow \mathbf{0.2} \text{SO}_2 \\ \mathbf{0.1} \end{array}$ <p>Total Oxygen required = 90.78 + 40 + 0.1 = 130.88</p> <p>Total oxygen required for 1000 kg of fuel = 130.88 x 10 = 1308.8 kg <i>(If calculation is done for 1 kg or 100 kg or 1000 kg full marks may be given)</i></p> <p>Oxygen already present in 1000 kg fuel (given) = 325 kg Additional Oxygen Required = 1308.8 - 325 = 983.8 Therefore quantity of dry air reqd. = (983.38) / 0.23 = 4270</p> <p>CO₂ generated per 1000 kg of fuel = 1247.8 kg H₂O generated per 1000 kg of fuel = 450 kg SO₂ generated per 1000 kg of fuel = 2 kg</p>																		

L6	<p>The management of a foundry is considering retrofitting the existing heat treatment furnace with hot face insulation of 75 mm ceramic fibre. (Note: Hot face insulation is known as veneering: ie over the existing refractory lining, ceramic fibre modules are applied to reduce the heat storage in refractory structure).</p> <p>Operating data:</p> <p>Heat Treatment furnace : (Bogey Type) Batch Operation Furnace Capacity : 5 Ton (per batch) Fuel type : Furnace Oil</p> <p>Area Side walls : $(1.4 \times 4.5) \times 2 = 12.6 \text{ m}^2$ Back Wall : $0.95 \times 1.4 = 1.33 \text{ m}^2$ Roof : $0.95 \times 4.5 = 4.3 \text{ m}^2$</p> <p>Refractory Type : Fire Bricks Wall Thickness Side walls : 18 inches Arch : 13.5 inches</p> <p>Number of cold starts per month: 10 Nos. Number of batches per month: 20 Nos. Fuel Cost : Rs 48/ kg GCV of furnace oil : 10200 kCal/kg</p> <p>Heat Storage (kCal /m²) for batch operation and cold start from walls and roof area are given below.</p> <table border="1"> <thead> <tr> <th rowspan="2"></th> <th colspan="2">For batch operation</th> <th colspan="2">Cold Start</th> </tr> <tr> <th>Existing(with only fire bricks)</th> <th>75 mm Veneering+ fire bricks</th> <th>Existing(with only fire bricks)</th> <th>75 mm Veneering+ fire bricks</th> </tr> </thead> <tbody> <tr> <td>Wall</td> <td>79480</td> <td>45350</td> <td>116697</td> <td>23,964</td> </tr> <tr> <td>Roof</td> <td>74770</td> <td>31,401</td> <td>97,236</td> <td>16,438</td> </tr> </tbody> </table> <p>For batch operation furnace is heated from 300°C to 850°C For cold start up furnace is heated from ambient 30 °C to 850°C</p> <p>Calculate the following due to veneering</p> <ol style="list-style-type: none"> Total heat loss reduction per month from wall and roof during batch operation. Total heat loss reduction per month from wall and roof during cold starts. 		For batch operation		Cold Start		Existing(with only fire bricks)	75 mm Veneering+ fire bricks	Existing(with only fire bricks)	75 mm Veneering+ fire bricks	Wall	79480	45350	116697	23,964	Roof	74770	31,401	97,236	16,438
	For batch operation		Cold Start																	
	Existing(with only fire bricks)	75 mm Veneering+ fire bricks	Existing(with only fire bricks)	75 mm Veneering+ fire bricks																
Wall	79480	45350	116697	23,964																
Roof	74770	31,401	97,236	16,438																
Ans	<p><u>Heat loss calculation for batch operation</u></p> <p>Heat reduction from Wall per m² = $79480 - 45350 = 34130 \text{ Kcal}$</p> <p>Heat reduction from total side wall & back wall = $34130 \times 13.93 = 475430.90 \text{ Kcal}$</p>																			

Heat reduction from roof per m ²	= 74770- 31401 =43369 Kcal
Heat reduction from total roof area	= 43369 x 4.3 = <u>186486.7</u> Kcal
Total heat reduction per batch from wall& roof	= 475430. 90 + 186486.7
	= 661917.60
Number of batches per month	= 20 Nos.
Total heat reduction per month from wall& roof	= 661917.6 x 20
	= 13238352 Kcals/month
<u>Heat loss calculation for</u> Cold Start	
Heat reduction from Wall per m ²	= 116697 - 23,964 = 92733 Kcal
Heat reduction from total side wall & back wall	= 92733 x13.93 = <u>1291770.69</u> Kcal
Heat reduction from roof per m ²	= 97,236 - 16,438 = 80798 Kcal
Heat reduction from total roof area	= 80798.5 x 4.3 = <u>347431.4</u> Kcal
Total heat reduction per batch from wall& roof	=1291770.69 + 347431
	=1639202.09
Number of cold starts per month	=10Nos.
Total heat reduction per month from wall& roof	= 16392020.9