



7.	Which of the following requires the largest amount of oxygen/kg of substance for combustion a) carbon      b) <u>hydrogen</u> c) sulphur      d) nitrogen
8.	Which of the following boiler utilizes the combination of suspension firing and grate firing a) traveling grate stoker boiler      b) packaged boiler c) <u>spreader stoker boiler</u> d) pulverized fuel boiler
9.	Which of the component is common to supercritical boiler and sub critical boiler for power generation a) economizer      b) water walls      c) re-heaters      d) <u>all of the above</u>
10.	The TDS level in boiler water for boiler blow down, is measured through a) alkalinity of water      b) thermal conductivity of water c) <u>electrical conductivity of water</u> d) turbidity of water
11.	NO <sub>x</sub> formation in FBC boilers is minimised because of a) higher velocity of flue gas in combustion chamber b) higher pressure of the air supplied c) <u>lower temperatures in the bed and combustion chamber</u> d) higher contact of solid particles in the flue gas
12.	The material used to control SO <sub>x</sub> in the FBC boiler is a) <u>limestone</u> b) alumina      c) silica      d) fly ash
13.	Condensate at pressure of 4 kg/cm <sup>2</sup> and 160°C temperature when exposed to atmosphere will a) become super heated      b) <u>partly convert to flash steam</u> c) remain as condensate      d) fully convert to flash steam
14.	As the pressure of water increases from 1kg/cm <sup>2</sup> to 8 kg/cm <sup>2</sup> , the values of enthalpy of steam and enthalpy of evaporation respectively a) increases & remains the same      b) <u>increases &amp; decreases</u> c) decreases & increases      d) decreases & remains the same
15.	The difference in temperature between steam and condensate is the principle of operation in a a) thermodynamic trap      b) <u>thermostatic trap</u> c) float trap      d) inverted bucket trap
16.	Scale losses in reheating furnaces will a) <u>increase with excess air</u> b) decrease with excess air c) have no relation with excess air      d) increase with CO in combustion gases
17.	The velocity of steam in steam pipe is directly proportional to a) number of bends in pipe      b) 5 <sup>th</sup> power of the diameter of pipe c) length of pipe      d) <u>specific volume of steam</u>
18.	Ceramic coating is used in furnaces because it enhances a) conductivity      b) convective heat transfer coefficient







	<p>(b) For fuels containing sulphur, low temperatures (below 160-170°C) of stack can lead to sulphur dew point corrosion. The main disadvantage of sulphur is the risk of corrosion by sulphuric acid formed during and after combustion, and condensing in cool parts of the chimney or stack, air preheater and economiser.</p> <p style="text-align: right;"><b>( 2.5 marks)</b></p>
S-2	<p>A steam pipe of 100mm diameter is insulated with mineral wool. As a part of energy saving measures, the insulation is upgraded with efficient Calcium silicate insulation. Calculate the percentage reduction in heat loss as a result of implementation of the above measure given the following data,</p> <p style="margin-left: 40px;">Boiler efficiency : 80%</p> <p style="margin-left: 40px;">Surface temperature with mineral wool : 95°C</p> <p style="margin-left: 40px;">Surface temperature with calcium silicate : 55°C</p> <p style="margin-left: 40px;">Ambient temperature : 25°C</p>
	<p>Ans:</p> <p>Heat loss thru non-insulated pipe = <math>[10 + (T_s - T_a) / 20] * (T_s - T_a)</math>  <math>T_s</math> = Surface temperature  <math>T_a</math> = Ambient temperature</p> <p>Heat loss thru non-insulated pipe = <math>[10 + (95 - 25) / 20] * (95 - 25)</math>          = 945 kcal/hr-m2 <span style="float: right;"><b>(2 marks)</b></span></p> <p>Heat los thru insulated pipe = <math>[10 + (55 - 25) / 20] * (55 - 25)</math>          = 345 kcal/hr-m2 <span style="float: right;"><b>(2 marks)</b></span></p> <p>% Reduction in heat loss = <math>(945 - 345) / 945</math>          = 63.5 % <span style="float: right;"><b>(1 mark)</b></span></p>
S-3	<p>Calculate the electricity consumption in an induction melting furnace from the following melt cycle data,</p> <p style="margin-left: 40px;">Mild steel (MS) scrap charged : 1250 kg</p> <p style="margin-left: 40px;">Specific heat of MS : 0.68 kJ/kg °C</p> <p style="margin-left: 40px;">Latent heat of MS : 270 kJ/kg</p> <p style="margin-left: 40px;">MS melting temperature : 1650 °C</p> <p style="margin-left: 40px;">Inlet MS charge temperature : 35 °C</p> <p style="margin-left: 40px;">Efficiency of furnace : 65%</p>
	<p>Ans:</p> <p style="margin-left: 40px;">Theoretical energy required for melting = <math>1250 (0.68 \times (1650 - 35) + 270)/3600</math></p>

	$= 475.1 \text{ kWh/hr or } 475.1 \text{ kw}$	<b>(3 marks)</b>																																													
	Actual energy input to the furnace $= 475.1 / 0.65$ Electricity consumption $= 730.9 \text{ Kwh/hr or } 730.9 \text{ kw}$	<b>(2 marks)</b>																																													
S-4	Paddy husk is being used as a combustion fuel in a water tube boiler. The ultimate analysis of fuel is given below. Calculate theoretical amount of air required per 100 kg of husk for the combustion from the following data																																														
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	<p style="text-align: right;"><b>(4 marks)</b></p> <p>Total Oxygen required = 93.04 kg oxygen / 100 kg fuel</p> <p>Therefore theoretical quantity of dry air reqd. = <math>93.04 / 0.23 = 404.5</math> kg air / 100 kg fuel (air contains 23% oxygen by wt.)</p> <p style="text-align: right;"><b>(1 mark)</b></p>
<p>S-5</p>	<p>Determine the Energy Utilization Factor (EUF) from the following back pressure cogeneration plant diagram and data given.</p> <div style="text-align: center;"> <p style="text-align: center;"><b>Back Pr Turbine Cogeneration Plant</b></p> </div>
	<p><b>Solution</b></p> <p>Input heat to turbine = <math>11,000 \times 760 = 8360000</math> Kcal/hr <span style="float: right;"><b>(1 mark)</b></span></p> <p>Useful heat to process Plant = <math>11,000 \times 650 - 170 = 5280000</math> Kcal/hr <span style="float: right;"><b>(1 mark)</b></span></p> <p>Useful Electrical output in alternator = <math>700 \times 860 = 602000</math> Kcal/hr <span style="float: right;"><b>(1 mark)</b></span></p> <p>Energy Utilization Factor (EUF) = <math>(602000 + 5280000) / 8360000</math> = 70.36% <span style="float: right;"><b>(2 marks)</b></span></p>
<p>S-6</p>	<p>For combustion of 500 kg/hr of Natural Gas containing 100% Methane, Calculate the percentage of CO<sub>2</sub> in the flue gas while 20% excess air is supplied.</p>



	<p>Ans:</p> $\text{CH}_4 + 2 \text{O}_2 \rightarrow \text{CO}_2 + 2\text{H}_2\text{O}$ <p>1 mole of Methane requires 2 moles of Oxygen.          16 Kg of Methane requires 64 Kg of Oxygen.          16 Kg of Methane produces 44 Kg of CO<sub>2</sub>.</p> <p>500 Kg/hr of Methane requires 2000 Kg/hr of Oxygen.          500 Kg/hr of Methane requires 1375 Kg/hr of CO<sub>2</sub></p> <p>Theoretical air required for combustion = <math>2000 / 0.23 = 8695 \text{ Kg/hr}</math> <span style="float: right;"><b>(2 marks)</b></span></p> <p>Considering 20% excess air,          Actual air supplied for combustion is <math>= 8695 * 1.2</math>  <math>= 10434 \text{ Kg/hr of air}</math> <span style="float: right;"><b>(1 mark)</b></span></p> <p>Flue gas generation with 20% excess air <math>= 500 + 10434</math>  <math>= 10934 \text{ Kg/hr}</math> <span style="float: right;"><b>(1 mark)</b></span></p> <p>% CO<sub>2</sub> in the flue gas <math>= 1375 / 10934</math>  <math>= 12.5 \%</math> <span style="float: right;"><b>(1 mark)</b></span></p>
<p>S-7</p>	<p>In a heat exchanger, steam is used to heat 3.0 KL/hr of furnace oil from 30°C to 100°C. The specific heat of furnace oil is 0.22 kCal/ kg/°C and the density of furnace oil is 0.95 gm/cc. How much steam per hour is needed if steam at 4 kg/cm<sup>2</sup> with latent heat of 510 kCal/ kg is used. If steam cost is Rs. 4.0/kg and electrical energy cost is Rs.8.0/kWh, which type of heating would be more economical in this particular case? (assume no losses in electrical and steam heating process)</p>
	<p>Ans: Total heat required <math>= m \text{ Cp } \Delta T</math>  <math>= (3 \times 1000 \times 0.95) \times 0.22 \times (100-30)</math>  <math>= 43890 \text{ kcal/hr}</math> <span style="float: right;"><b>(1.5 mark)</b></span></p> <p>a) Amount of steam required <math>= 43890/510</math>  <math>= 86 \text{ kg/hr}</math>          Steam cost <math>= 86 \times \text{Rs.}4</math>  <math>= \text{Rs.} 344/\text{hr}</math> <span style="float: right;"><b>(1.5 marks)</b></span></p> <p>b) Amount of electricity required <math>= 43890/860</math>  <math>= 51 \text{ kWh}</math>  <math>= 51 \times \text{Rs.} 8</math>  <math>= \text{Rs.}486/ \text{hr}</math>          Steam heating will be more economical <span style="float: right;"><b>(2 marks)</b></span></p>

S-8	<p>In a sugar mill, a process requires 5 000 kg/hr of dry saturated steam at 7 kg/cm<sup>2</sup> (g). For the flow velocity not to exceed 25 m/s, determine the pipe diameter size for distribution of steam.                  Specific volume at 7 kg/cm<sup>2</sup> = 0.24 m<sup>3</sup>/kg</p>
	<p>Ans.</p> <p>The velocity of steam maximum = 25 m/s                  Specific volume at 7 kg/cm<sup>2</sup> = 0.24 m<sup>3</sup>/kg</p> <p>Mass flow rate = 5000 kg/hr                  = 5000/3600 = 1.389 kg/sec</p> <p>Volumetric flow = 1.389 x 0.24 = 0.333 m<sup>3</sup>/sec <span style="float: right;">(1 mark)</span></p> <p>Volumetric flow rate(m<sup>3</sup>/s) = Velocity (m/s) x cross sectional area (m<sup>2</sup>) <span style="float: right;">(1 mark)</span></p> <p>Therefore,</p> $D = \sqrt{\frac{4 \times \text{Volumetric flowrate}}{\pi \times \text{Flow velocity}}}$ $D = \sqrt{\frac{4 \times 0.333}{\pi \times 25}}$ $D = 0.130 \text{ m or } 130 \text{ mm}$ <p>Since the steam velocity must not exceed 25 m/s, the pipe size must be at least 130 mm; the nearest commercially available size, 150 mm, would be selected. <span style="float: right;">(3 marks)</span></p>

----- End of Section - II -----

Section - III: LONG DESCRIPTIVE QUESTIONS

Marks: 6 x 10 = 60

- (i) Answer all SIX questions
- (ii) Each question carries **Ten** marks

L-1	<p>A liquid waste stream has a flow rate of 3.5 kg/s and a temperature of 75°C with a specific heat capacity of 4190 J/kgK. Heat recovered from the hot waste stream is used to pre-heat boiler make-up water. The flow rate of the make-up water is 2.8 kg/s, its temperature is 12°C and its specific heat capacity is 4190 J/kg/K. The overall heat transfer coefficient of the heat exchanger is 800 W/m<sup>2</sup>K. If a make-up water exit temperature of 50°C is required, and assuming that there are no heat loss from the heat losses from the exchanger, determine</p> <ol style="list-style-type: none"> <li>1) The heat transfer rate</li> <li>2) The exit temperature of the effluent and</li> <li>3) The area of the heat exchanger required</li> </ol>
	<p><b>Solution</b></p> <p>i) Heat gained by makeup water = <math>Q_c = m_c c_c \Delta T = 2.8 \times 4190 \times (50-12)</math>  <math>= 445816 \text{ W} = 445.82 \text{ kW}</math> <span style="float: right;"><b>(2 marks)</b></span></p> <p>ii) <math>m_h c_h (t_{h1} - t_{h2}) = m_c c_c (t_{c1} - t_{c2})</math></p> <p><math>3.5 \times 4190 \times (75 - t_{h2}) = 2.8 \times 4190 \times (50 - 12)</math>  <math>t_{h2} = 44.6 \text{ }^\circ\text{C}</math> <span style="float: right;"><b>(3 marks)</b></span></p> <p>iii) Now because the water outlet temperature is above the outlet temperature of the effluent a counter-flow heat exchanger is required</p> <div style="text-align: center;"> <p><b>Counter Flow Arrangement</b></p> </div> $\text{LMTD} = \frac{\Delta t_1 - \Delta t_2}{\ln \left( \frac{\Delta t_1}{\Delta t_2} \right)}$ $= \frac{(75-50)-(44.6-12)}{\ln (75-50)/(44.6-12)}$ $= \frac{25-32.4}{\ln(25/32.4)}$ <p>LMTD = 28.54°C <span style="float: right;"><b>(2.5 marks)</b></span></p>

	$Q = UA \text{ (LMTD)}$ $= \frac{445816}{800 \times 28.54}$ <p style="text-align: center;">Area = 19.5 m<sup>2</sup></p> <p style="text-align: right;"><b>(2.5 marks)</b></p>
L-2	<p>Oil fired Boiler is generating 100 TPH of steam at 85% efficiency, operating 330 days in a year. Management has installed a water treatment plant at Rs 2 Crore investment for reducing the TDS in boiler feed from 450 ppm to 150 ppm. The maximum permissible limit of TDS in the boiler is 3000 ppm and make up water is 10%. Temperature of blowdown water is 175°C and boiler feed water temperature is 45°C. Calorific value of Fuel oil is 10200 Kcal/kg.</p> <p>Calculate the payback period if the cost of fuel is Rs.34500 per ton.</p>
	<p>Ans:</p> $\text{Blow down \%} = \frac{\text{Feed water TDS} \times \% \text{ make up water}}{(\text{maximum permissible TDS in boiler water} - \text{Feed water TDS})} \times 100$ <p>Initial blow down = 450 * 10 / (3000 – 450) Initial blow down = 1.76 %</p> <p>Improved blow down = 150 * 10 / (3000 – 150) Improved blow down = 0.53 %</p> <p>Reduction in blow down = 1.76 – 0.53 Reduction in blow down = 1.24 %</p> <p>Reduction in blow down = 1.24 * 100 * 1000 / 100 Reduction in blow down = 1238 kg/hr</p> <p style="text-align: right;"><b>(4 marks)</b></p> <p>Specific heat of water is 1 kcal/kg°C</p> <p>Heat savings = m * Cp * (T<sub>1</sub> – T<sub>2</sub>) = 1238 * 1 * (175 – 45) Heat savings = 160991 kcal/hr</p> <p>Fuel Oil saving = 160991 / (10200 * 0.85) = 18.6 kg/hr = 18.6 * 24 * 330 / 1000 = 147.1 MT / annum</p> <p>Fuel Oil cost savings = 147.1 * 345000 = Rs. 50.75 lakh</p> <p style="text-align: right;"><b>(4 marks)</b></p> <p>Investment on water treatment plant = Rs. 2 Crore</p> <p>Payback period = 2 / 0.5075 Payback period = 3.9 years (or) 47 months</p> <p style="text-align: right;"><b>(2 marks)</b></p>

<p>L-3</p>	<p>As a part of energy conservation measure, APH (Air Pre-heater) is installed in a fired heater. The APH is designed to pre-heat 240 m<sup>3</sup>/min of combustion air to 250°C. Flue gas enters the APH at 375°C. Calculate the flue gas leaving the stack and also determine the improvement in furnace efficiency after the installation of APH with the following data</p> <p>Density of air : 1.15 kg/m<sup>3</sup>          Specific heat of air : 0.23 Kcal/kg°C          Specific heat of flue gas : 0.26 Kcal/kg°C          Calorific value of fuel : 9850 Kcal/kg          Air to fuel ratio : 17          Efficiency of furnace : 69 %          Ambient temperature : 30°C</p>
	<p><b>Solution:</b></p> <p>Amount of Air flow = 240 * 60 * 1.15          = 16560 Kg/hr <span style="float: right;"><b>(1 mark)</b></span></p> <p>Amount of fuel = 16560 / 17          = 974.12 Kg/hr <span style="float: right;"><b>(1 mark)</b></span></p> <p>Amount of flue gas = 16560 + 974.12          = 17534.1 Kg/hr <span style="float: right;"><b>(1 mark)</b></span></p> <p>Heat absorbed by combustion air = 16560 * 0.23 * (250 – 30)          = 837936 Kcal/hr <span style="float: right;"><b>(1.5 mark)</b></span></p> <p>Temperature difference in flue gas = 837936 / (17534.1 * 0.26)          = 183.8 °C <span style="float: right;"><b>(1.5 mark)</b></span></p> <p>Flue gas leaves the stack at temp = 375 – 183.8 = 191.2 °C <span style="float: right;"><b>(1 mark)</b></span></p> <p>Efficiency of APH = heat absorbed by air / Heat input * 100          = 837936 * 100 / (974.12* 9850)          = 8.73 % <span style="float: right;"><b>(2 marks)</b></span></p> <p>Overall efficiency after APH = 69 + 8.73 % = 77.73 % <span style="float: right;"><b>(1 mark)</b></span></p>
<p>L-4</p>	<p>Write short notes on any two of the following: <span style="float: right;"><b>(5 marks each)</b></span></p> <p>a) Plate heat exchanger <span style="float: right;">(page 242 of book-2)</span></p> <p>b) Multiple effect evaporator <span style="float: right;">(page 247-248 of book-2)</span></p> <p>c) Gas turbine cogeneration system <span style="float: right;">(page 192 of book-2)</span></p>

L-5	<p>a) Find out the efficiency of the furnace oil fired boiler by the direct method in an agro product manufacturing plant given the following data:</p> <table style="width: 100%; border: none;"> <tr> <td>Type of boiler</td> <td>: Furnace oil fired</td> </tr> <tr> <td>Quantity of steam (dry) generated</td> <td>: 5 TPH</td> </tr> <tr> <td>Steam pressure / temp</td> <td>: 10 kg/cm<sup>2</sup>(g)/ 180 °C</td> </tr> <tr> <td>Quantity of oil consumed</td> <td>: 0.350 TPH</td> </tr> <tr> <td>Feed water temperature</td> <td>: 75 °C</td> </tr> <tr> <td>GCV of Furnace oil</td> <td>: 10300 kCal/kg</td> </tr> <tr> <td>Enthalpy of saturated steam at 10 kg/cm<sup>2</sup> pressure</td> <td>: 665 kCal/kg</td> </tr> <tr> <td>Enthalpy of feed water</td> <td>: 75 kCal/kg</td> </tr> <tr> <td>Cost of furnace oil</td> <td>: Rs 32/kg</td> </tr> <tr> <td>Annual operating hours</td> <td>: 7200 hrs /year</td> </tr> </table> <p>b) The oil fired boiler was converted to coconut shell firing maintaining the same steam and feed water parameters.</p> <p>i) Determine the fuel consumption per hour                  ii) Return on investment for the conversion scheme.</p> <table style="width: 100%; border: none;"> <tr> <td>Fuel fired in the boiler</td> <td>: coconut shell fuel</td> </tr> <tr> <td>GCV of coconut shell</td> <td>: 4200 kCal/kg</td> </tr> <tr> <td>Efficiency with coconut shell firing</td> <td>: 76%</td> </tr> <tr> <td>Cost of coconut shell</td> <td>: Rs 12/kg</td> </tr> <tr> <td>Annual operating hours</td> <td>: 7200 hrs /year</td> </tr> <tr> <td>Investment towards boiler conversion</td> <td>: Rs 50 lakhs</td> </tr> <tr> <td>Annual interest on capital</td> <td>: Rs 6 lakhs /yr</td> </tr> </table>	Type of boiler	: Furnace oil fired	Quantity of steam (dry) generated	: 5 TPH	Steam pressure / temp	: 10 kg/cm <sup>2</sup> (g)/ 180 °C	Quantity of oil consumed	: 0.350 TPH	Feed water temperature	: 75 °C	GCV of Furnace oil	: 10300 kCal/kg	Enthalpy of saturated steam at 10 kg/cm <sup>2</sup> pressure	: 665 kCal/kg	Enthalpy of feed water	: 75 kCal/kg	Cost of furnace oil	: Rs 32/kg	Annual operating hours	: 7200 hrs /year	Fuel fired in the boiler	: coconut shell fuel	GCV of coconut shell	: 4200 kCal/kg	Efficiency with coconut shell firing	: 76%	Cost of coconut shell	: Rs 12/kg	Annual operating hours	: 7200 hrs /year	Investment towards boiler conversion	: Rs 50 lakhs	Annual interest on capital	: Rs 6 lakhs /yr
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	<p><b>Solution:</b></p> <p>a) Efficiency of furnace oil fired boiler (Direct method)</p> <table style="width: 100%; border: none;"> <tr> <td style="width: 40%;">Boiler Efficiency (<math>\eta</math>)</td> <td style="width: 40%;"><math>= 5000 \times (665-75) / (350 \times 10300)</math></td> <td style="width: 20%;"></td> </tr> <tr> <td>Boiler efficiency</td> <td><math>= 81.8\%</math> (on GCV basis)</td> <td style="text-align: right;"><b>(2.5 marks)</b></td> </tr> </table> <p>b) i) Coconut shell fuel consumption after conversion:</p> <table style="width: 100%; border: none;"> <tr> <td style="width: 40%;">Fuel consumption</td> <td style="width: 40%;"><math>= 5000 \times (665-75) / (0.76 \times 4200)</math></td> <td style="width: 20%;"></td> </tr> <tr> <td></td> <td><math>= 924.2</math> kg/hr</td> <td style="text-align: right;"><b>(2.5 marks)</b></td> </tr> </table> <p>ii) ROI for the conversion scheme</p> <p>Annual fuel cost of furnace oil fired boiler = <math>350 \times 7200 \times 32 =</math> Rs 8,06,40,000 /year <span style="float: right;"><b>(1 mark)</b></span></p> <p>Annual fuel cost of coconut shell fired boiler = <math>924.2 \times 7200 \times 12 =</math> Rs 7,98,50,880/year <span style="float: right;"><b>(1 mark)</b></span></p> <p>Annual net monetary savings after conversion</p> <p><math>= \frac{[(8,06,40,000 - 7,98,50,880) - 6,00,000]}{50,00,000} \times 100</math></p> <p><math>= 3.8\%</math> <span style="float: right;"><b>(3 marks)</b></span></p>	Boiler Efficiency ( $\eta$ )	$= 5000 \times (665-75) / (350 \times 10300)$		Boiler efficiency	$= 81.8\%$ (on GCV basis)	<b>(2.5 marks)</b>	Fuel consumption	$= 5000 \times (665-75) / (0.76 \times 4200)$			$= 924.2$ kg/hr	<b>(2.5 marks)</b>																						
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	$= 924.2$ kg/hr	<b>(2.5 marks)</b>																																	

<p>L-6</p>	<p>a. State two examples of heat pump applications                  b. In which situation are heat pumps most promising                  c. Draw the schematics of a heat pump system                  d. Briefly discuss each sub process stage of the heat pump system</p>
	<p>a) heat pump applications</p> <ul style="list-style-type: none"> <li>i) space heating system</li> <li>ii) use in plastic factory where chilled water is used to cool injection moulding machines, and</li> <li>iii) drying applications such as maintaining dry atmosphere in storage and drying compressed air</li> </ul> <p style="text-align: right;"><b>(2 marks)</b></p> <p>b) In a situation when both the cooling and heating capabilities of the cycle can be used in combination</p> <p style="text-align: right;"><b>(2 marks)</b></p> <p>c) Schematic of a heat pump system:</p> <div data-bbox="395 891 1426 1487" data-label="Diagram"> </div> <p style="text-align: center;"><b>Heat Pump Arrangement</b></p> <p style="text-align: right;"><b>(2 marks)</b></p> <p>Step 1: In the evaporator the heat is extracted to boil the circulating working fluid                  Step 2: The evaporated working fluid is compressed in a compressor rising working fluid temperature and pressure                  Step 3: The heat is delivered to the condenser                  Step 4: The pressure of the working fluid is reduced in a throttling valve and condensate returned to the compressor</p> <p style="text-align: right;"><b>(4 marks)</b></p>

..... **End of Section – III** .....